

# Simultaneous Removal of NO<sub>x</sub> and Hg in a Low Temperature Selective Catalytic and Adsorptive Reactor

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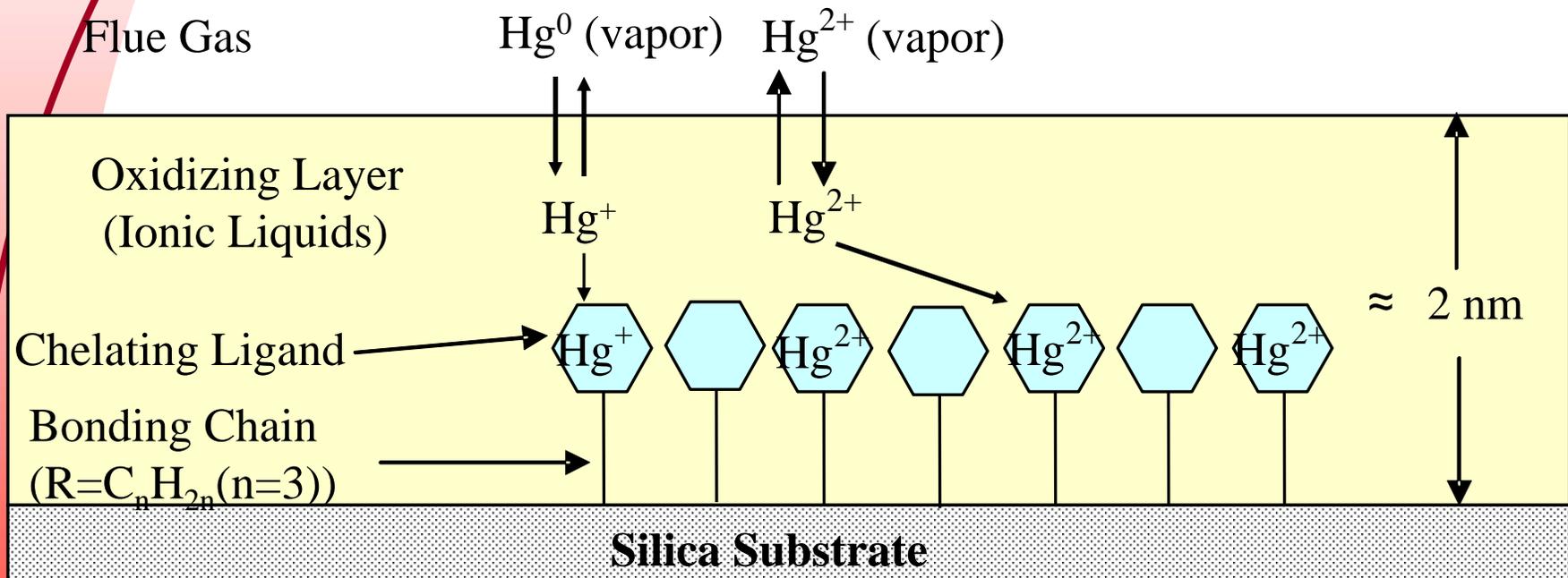
University of Cincinnati, Cincinnati, OH, 45221

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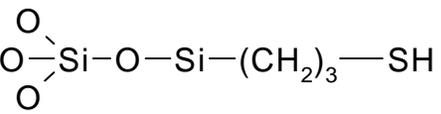
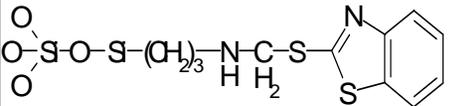
# Thermally Stable Chelating Adsorbents for $\text{Hg}^{2+}$ and $\text{Hg}^0$ Capture

**Adsorption Group**  
**Lei Ji, Stephen W. Thiel & Neville G. Pinto**

## Chelating Adsorbent

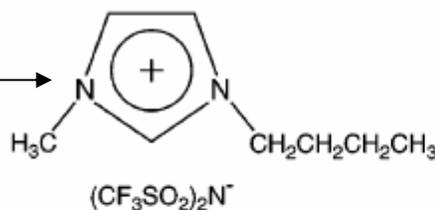


## Chelating Ligands

Chelating Ligand	Chemical Structure	Active Sites Concentration	BET Area (Support+ Ligand)	Theoretical Hg <sup>2+</sup> Ligand Capacity	T <sub>max</sub>
		mmol/g	m <sup>2</sup> /g	(mg/g)	°C
Pure Silica	-	-	283	-	-
MPTS (3-mercaptopropyltrimethoxysilane)	 $\begin{array}{c} \text{O} \\ \diagdown \\ \text{O}-\text{Si}-\text{O}-\text{Si}-(\text{CH}_2)_3-\text{SH} \\ \diagup \\ \text{O} \end{array}$	0.58	259	117 (1:1)	200
APTS-MBT (Mercaptobenzothiazole)	 $\begin{array}{c} \text{O} \\ \diagdown \\ \text{O}-\text{S}-\text{O}-\text{S}-(\text{CH}_2)_3-\text{N}-\text{C}-\text{S} \\ \diagup \\ \text{O} \quad \quad \quad \text{H} \quad \text{H}_2 \end{array}$	0.22	245	22 (2:1)	190

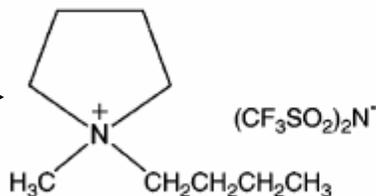
# Ionic Liquids Screened

1-butyl-3-methylimidazolium  
[bmim]

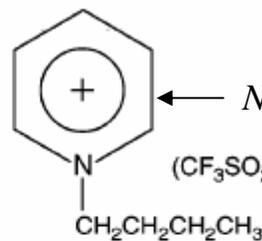


[bmim][ $(\text{CF}_3\text{SO}_2)_2\text{N}$ ]

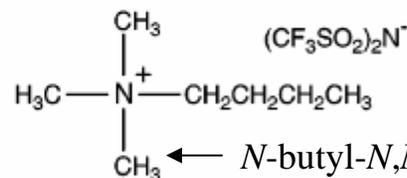
*N*-butyl-*N*-methylpyrrolidinium  
[bmpro]



[bmpro][ $(\text{CF}_3\text{SO}_2)_2\text{N}$ ]



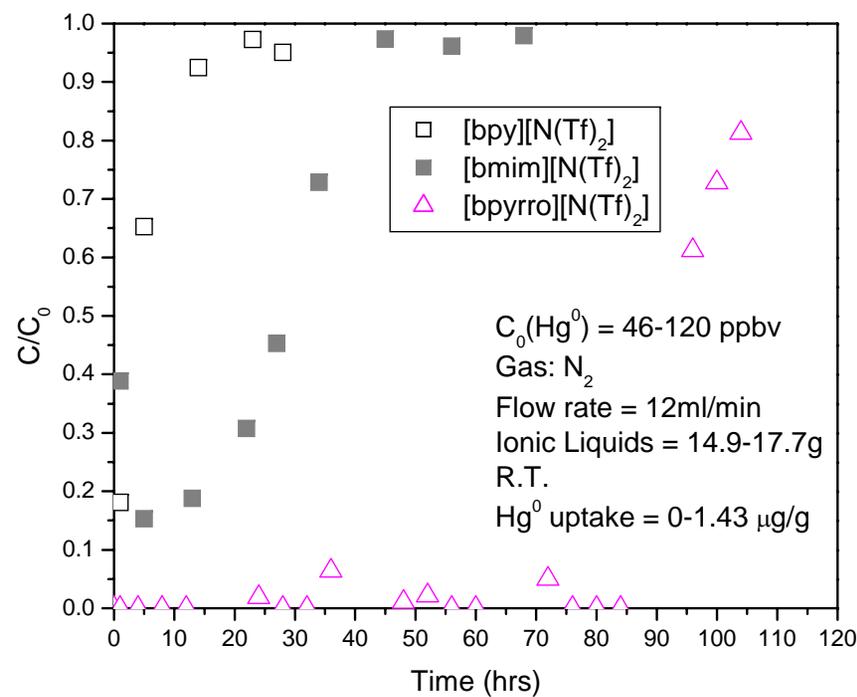
[bpy][ $(\text{CF}_3\text{SO}_2)_2\text{N}$ ]



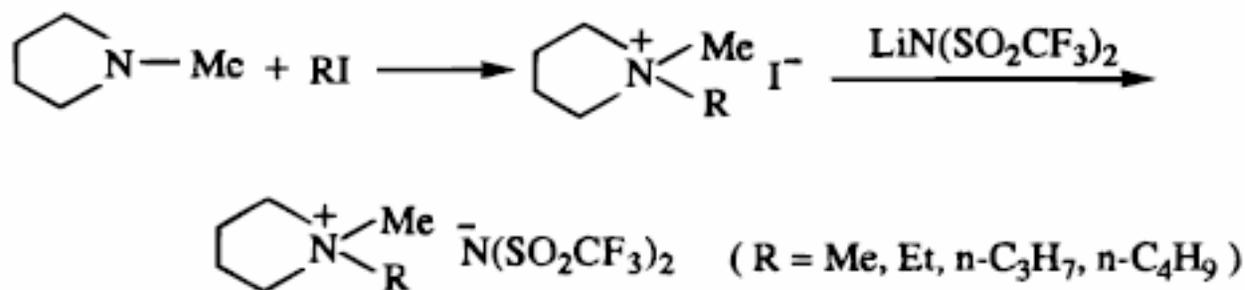
[ $(n\text{-C}_4\text{H}_9)(\text{CH}_3)_3\text{N}$ ][ $(\text{CF}_3\text{SO}_2)_2\text{N}$ ]

Same Anion: bis(trifluoromethane sulfonyl)imide  
[ $(\text{CF}_3\text{SO}_2)_2\text{N}$ ]

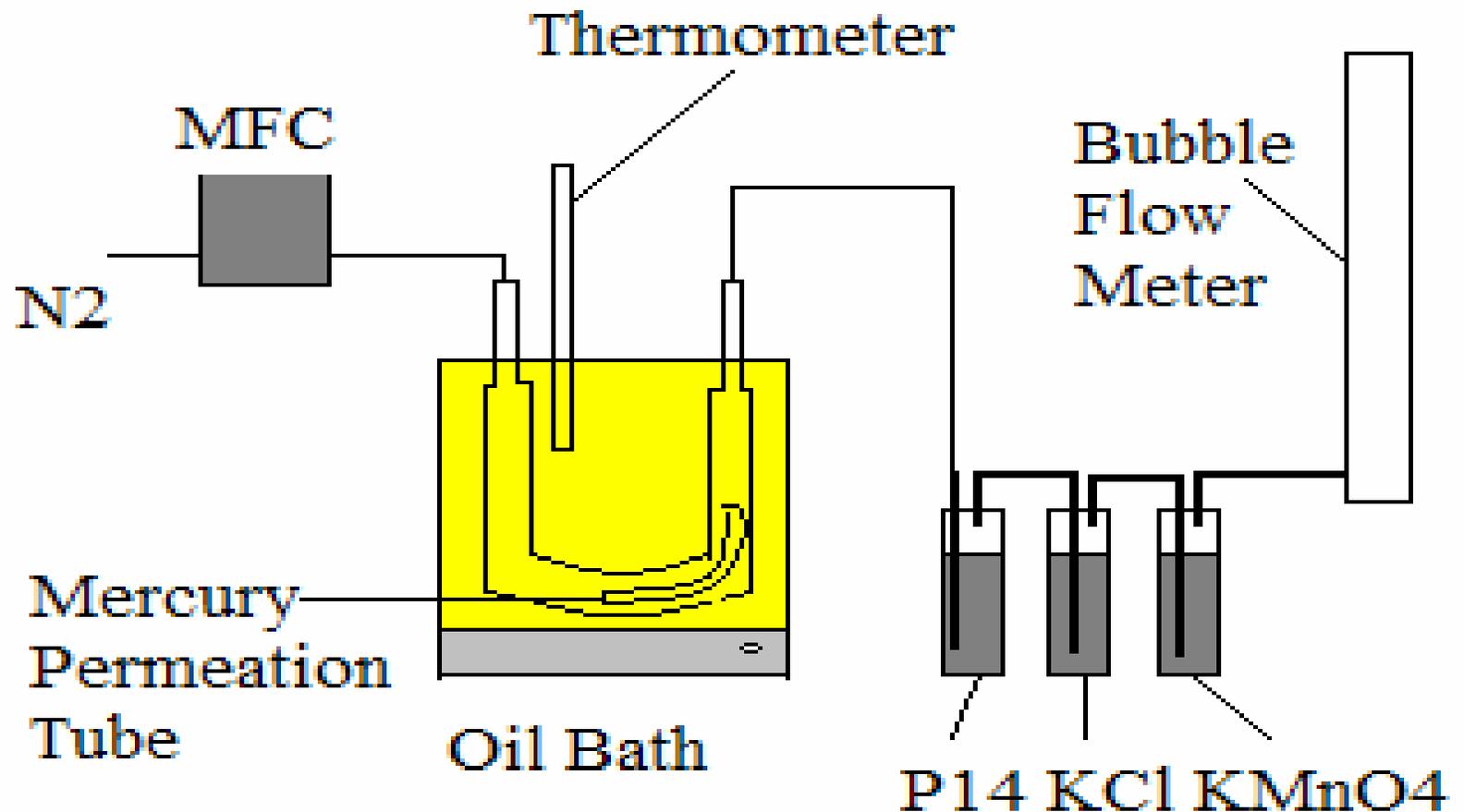
# Effect of Cation of Ionic Liquids Coating on Mercury Capture



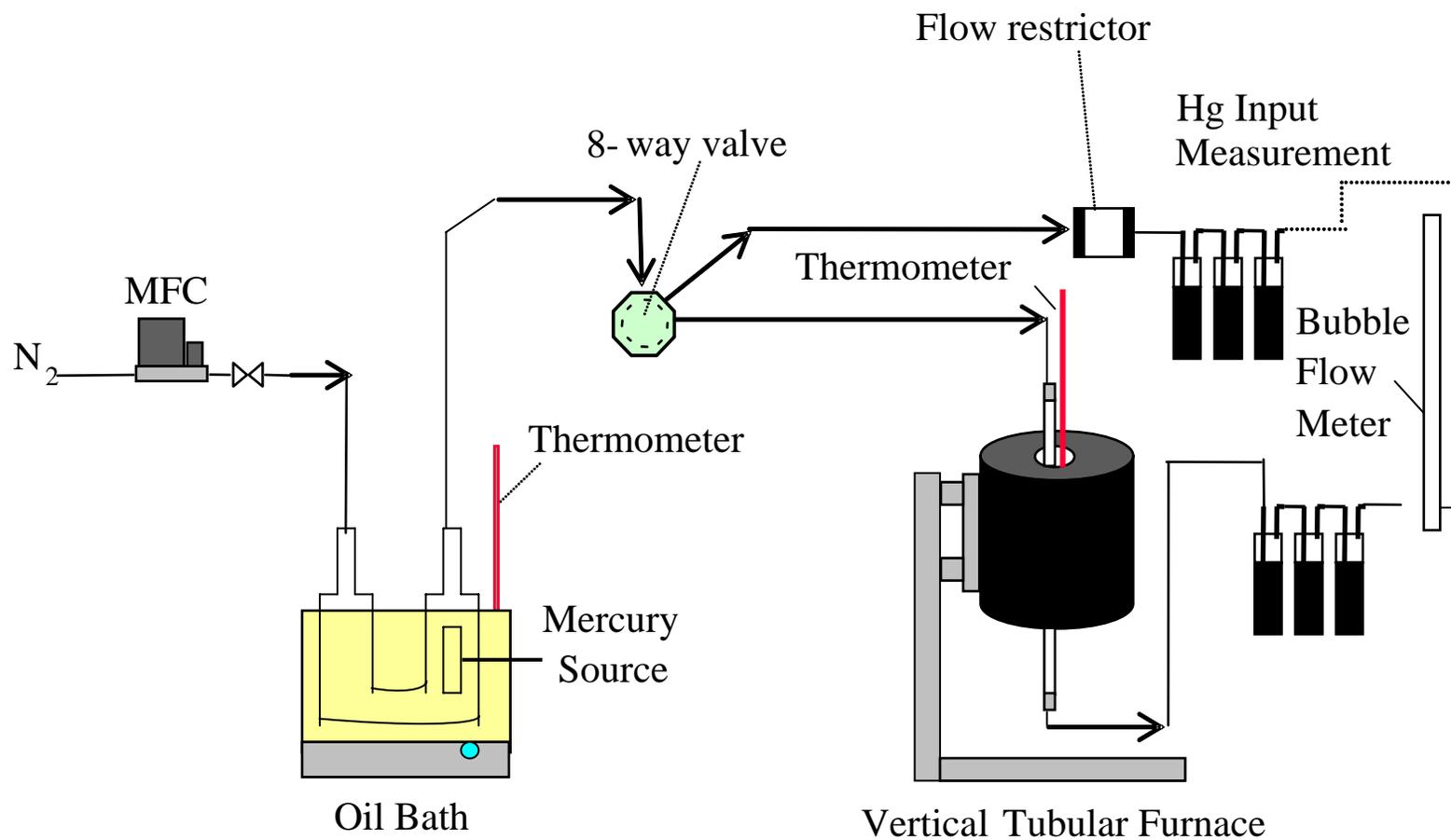
# $P_{14}$ : 1-butyl-1-methyl pyrrolidinium bis(trifluoromethane sulfonyl)imide



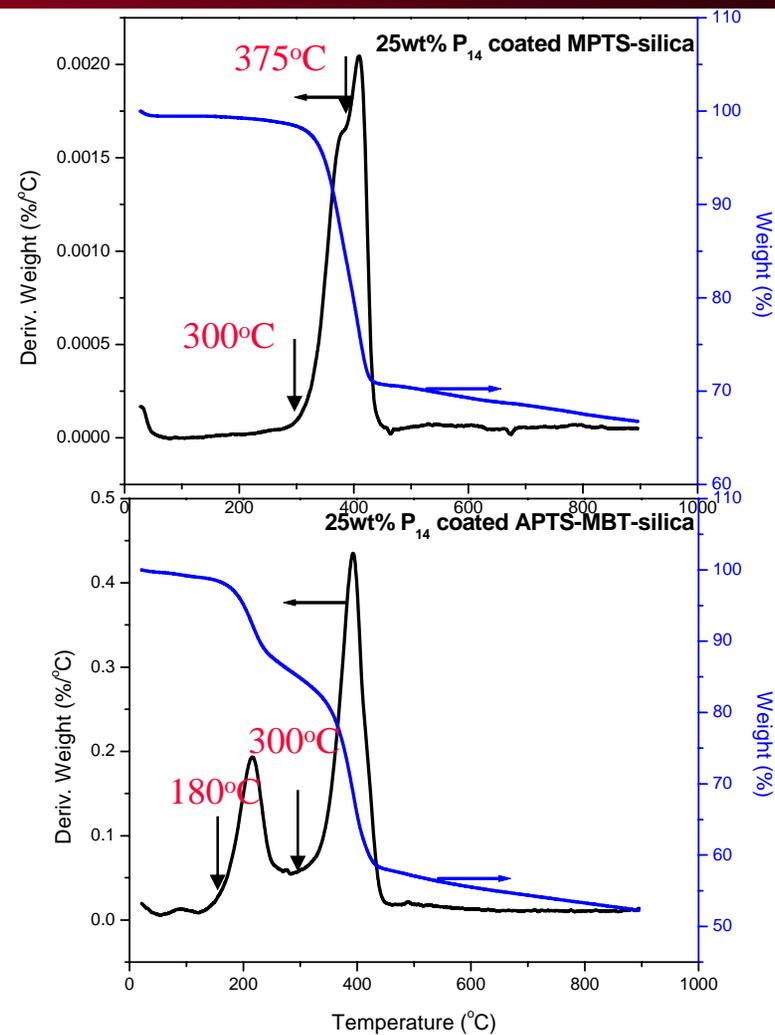
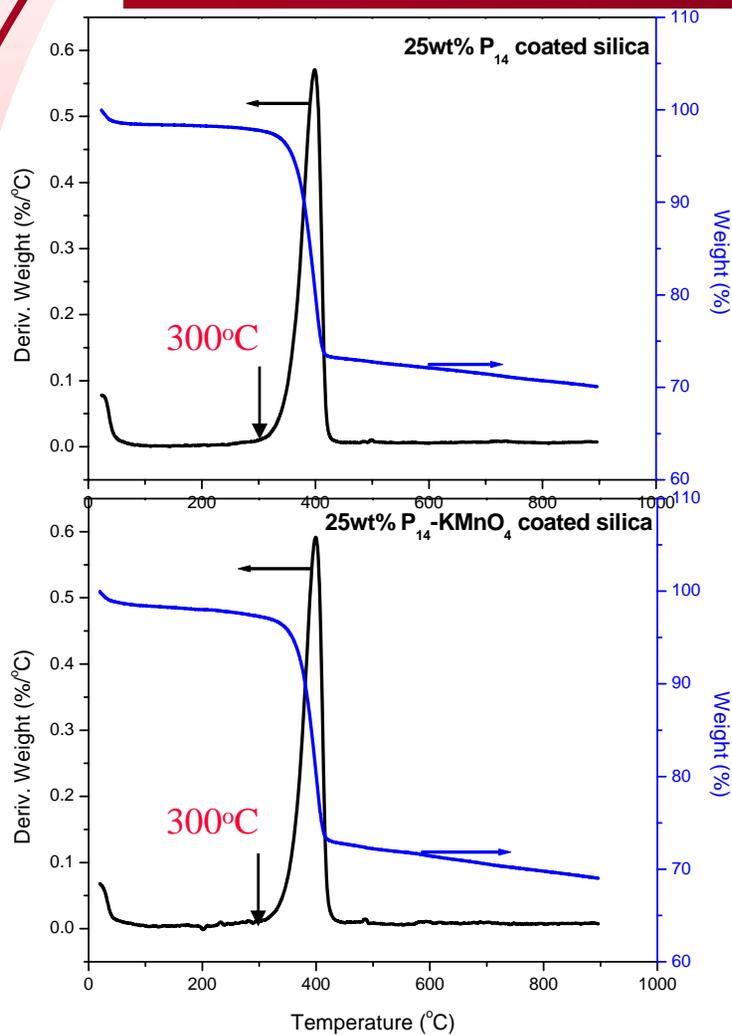
## Apparatus (Bulk Phase)



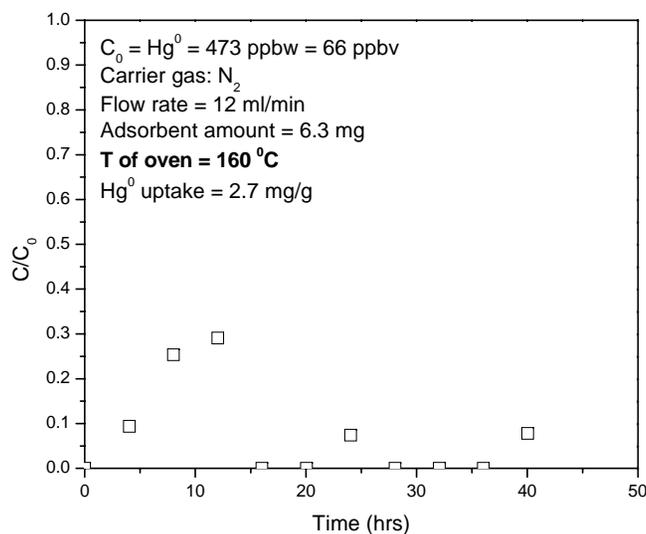
# Apparatus (Fixed Bed)



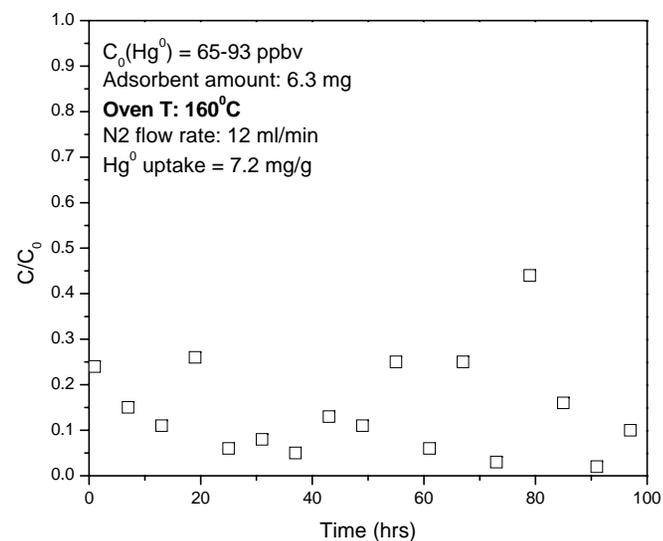
# Thermal Stability



# Mercury Capture Performance (Fixed-Bed at 160°C)



25 wt%  $\text{P}_{14}$  coated silica



25 wt%  $\text{P}_{14}\text{-KMnO}_4$  coated MPTS-silica

## Summary

- $P_{14}$  and  $P_{14}$ - $KMnO_4$  are promising ionic liquids for  $Hg^0$  capture
- $P_{14}$  and  $P_{14}$ - $KMnO_4$  are stable up to  $300^\circ C$
- High  $Hg^0$  uptake at  $160^\circ C$ , several times higher than that of activated carbon
- Very rapid  $Hg^0$  uptake, 0.04 seconds empty bed gas residence time
- The MPTS (3-mercaptopropyltrimethoxy-silane) chelating ligand was found to be the most effective than APTS-MBT (mercaptobenzo-thiazole)

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# TiO<sub>2</sub> Supported MnO<sub>2</sub> DeNO<sub>x</sub> Catalyst for Hg<sup>0</sup> Capture

**Adsorption Group**

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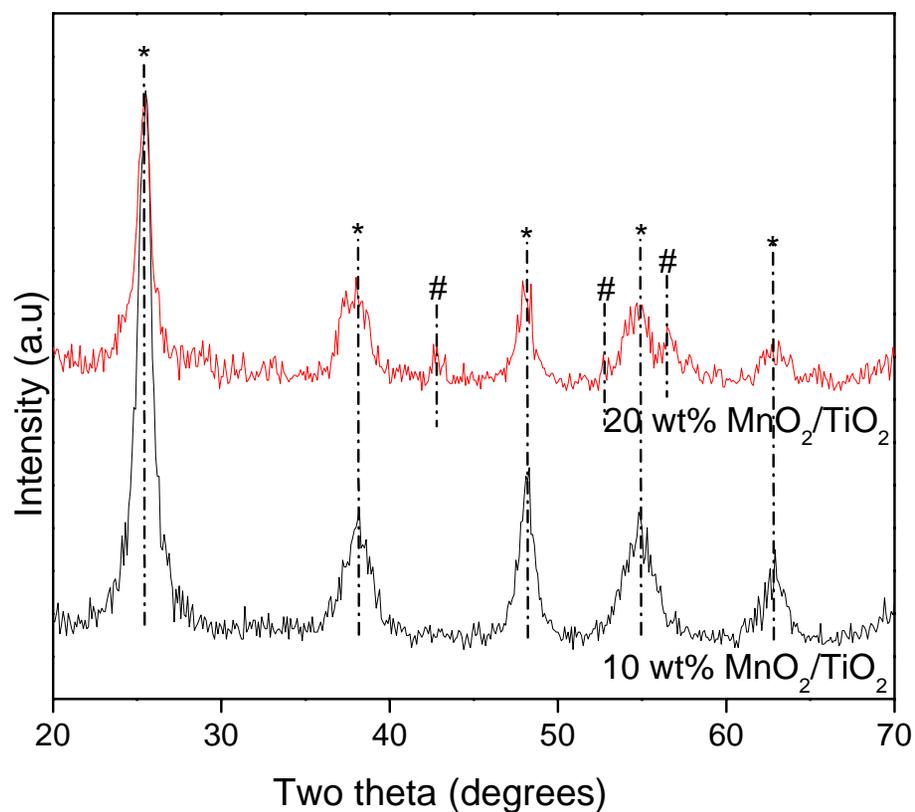
**Catalysis Group**

**Pavani M. Sreekanth, Peter G. Smirniotis**

## BET Surface Area and Total Acidity of $\text{MnO}_2/\text{TiO}_2$ Catalysts

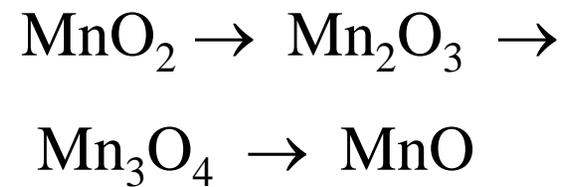
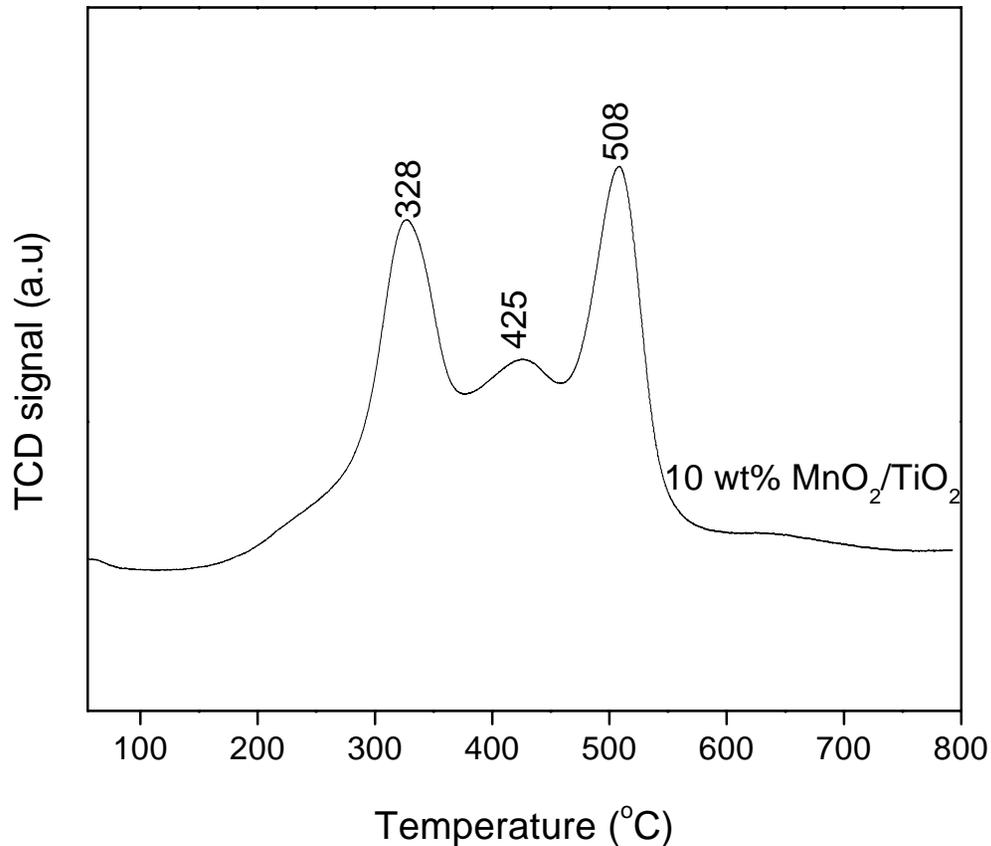
Sample	BET surface area ( $\text{m}^2/\text{g}$ )	Total Acidity ( $\text{ml g}^{-1}$ )
$\text{TiO}_2$	309	-
10 wt% $\text{MnO}_2/\text{TiO}_2$	236	21
20 wt% $\text{MnO}_2/\text{TiO}_2$	198	23.2

## Powder XRD patterns for MnO<sub>2</sub>/TiO<sub>2</sub> SCR catalysts

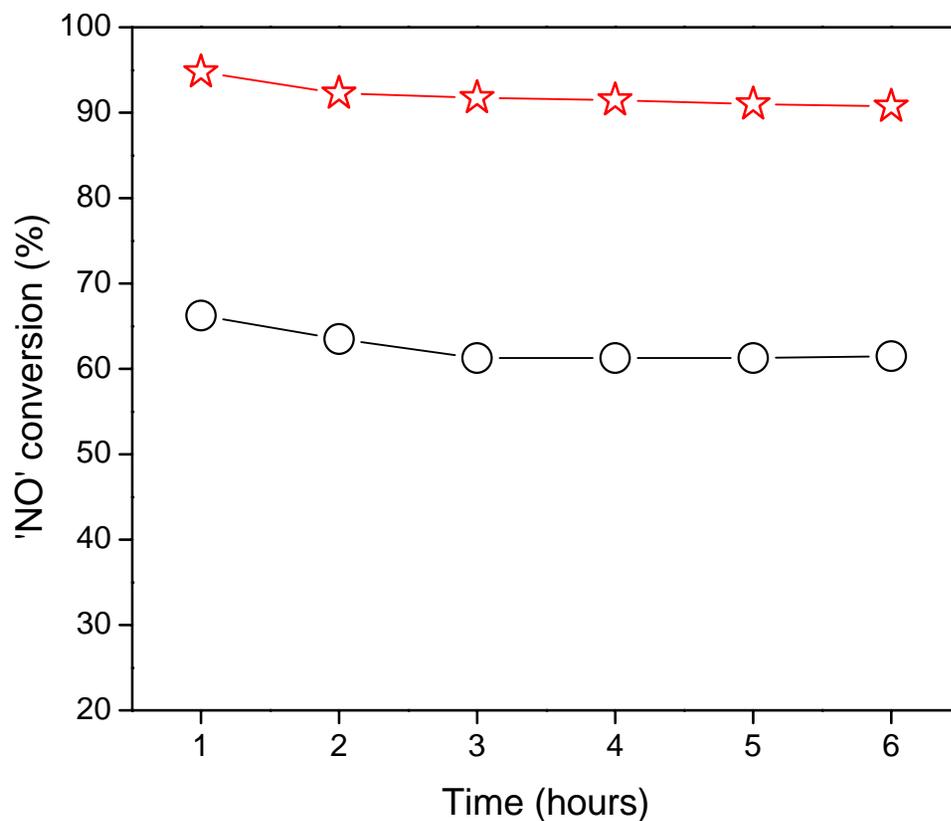


- ❖ (\*) anatase TiO<sub>2</sub>
- ❖ (#) MnO<sub>2</sub>

## TPR pattern of 10 wt% MnO<sub>2</sub>/TiO<sub>2</sub> catalyst

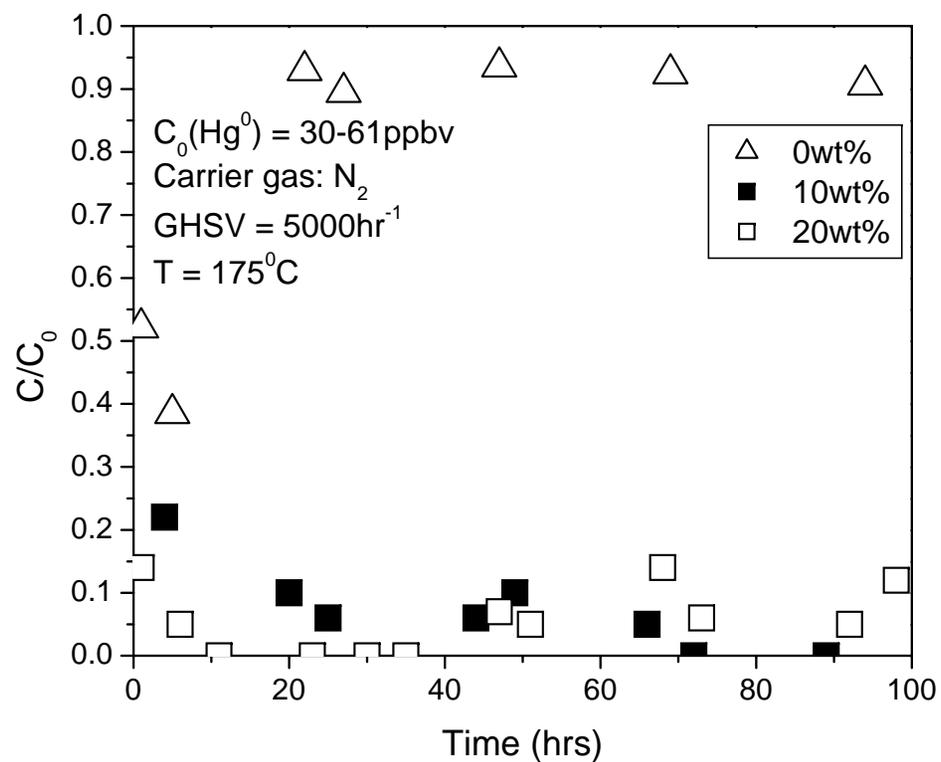


## SCR of NO using CO as a reductant over 10 wt% MnO<sub>2</sub>/TiO<sub>2</sub> catalyst

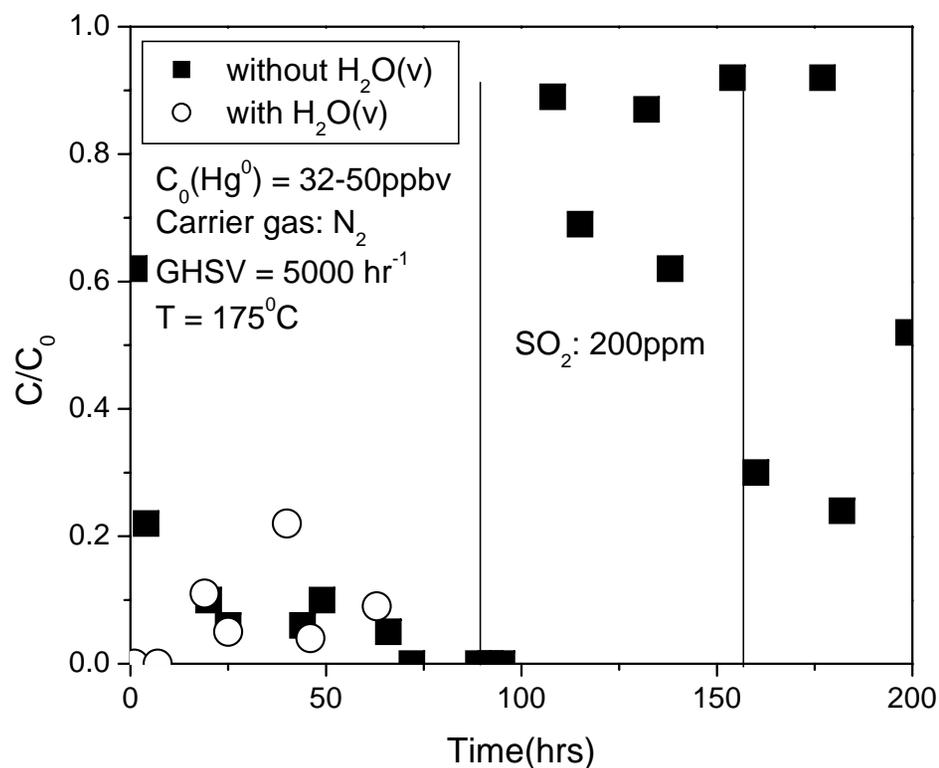


(○) 175 °C; (☆) 200 °C;  
NO = CO = 400 ppm;  
Oxygen = 2 vol%

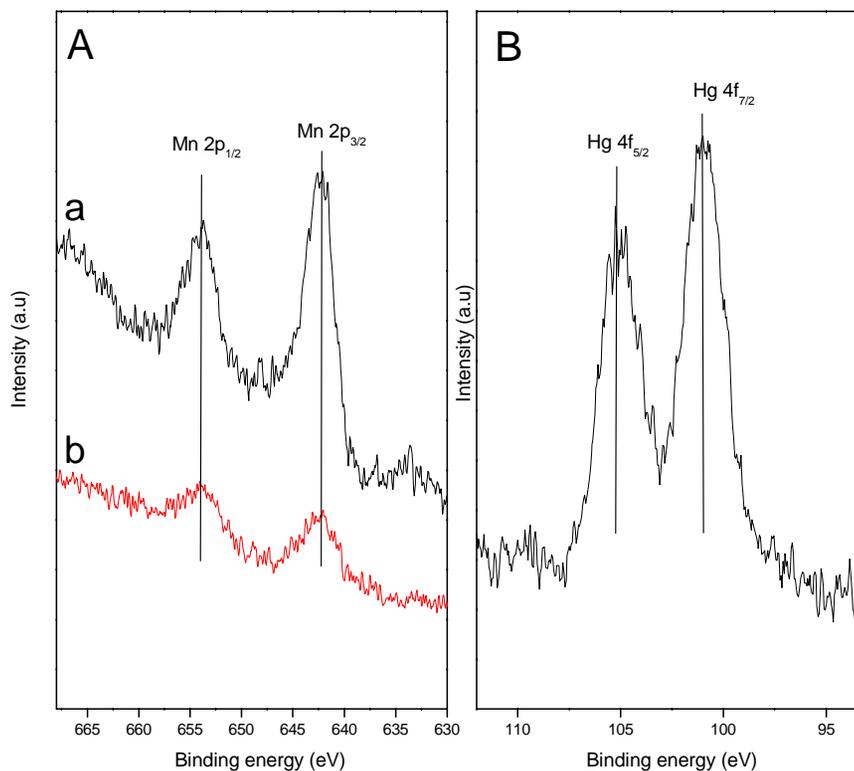
# Influence of $\text{MnO}_2$ Loading on Mercury Capture Behavior



# Effect of SO<sub>2</sub> and Water Vapor on Mercury Capture Behavior using 10wt% MnO<sub>2</sub> Catalyst

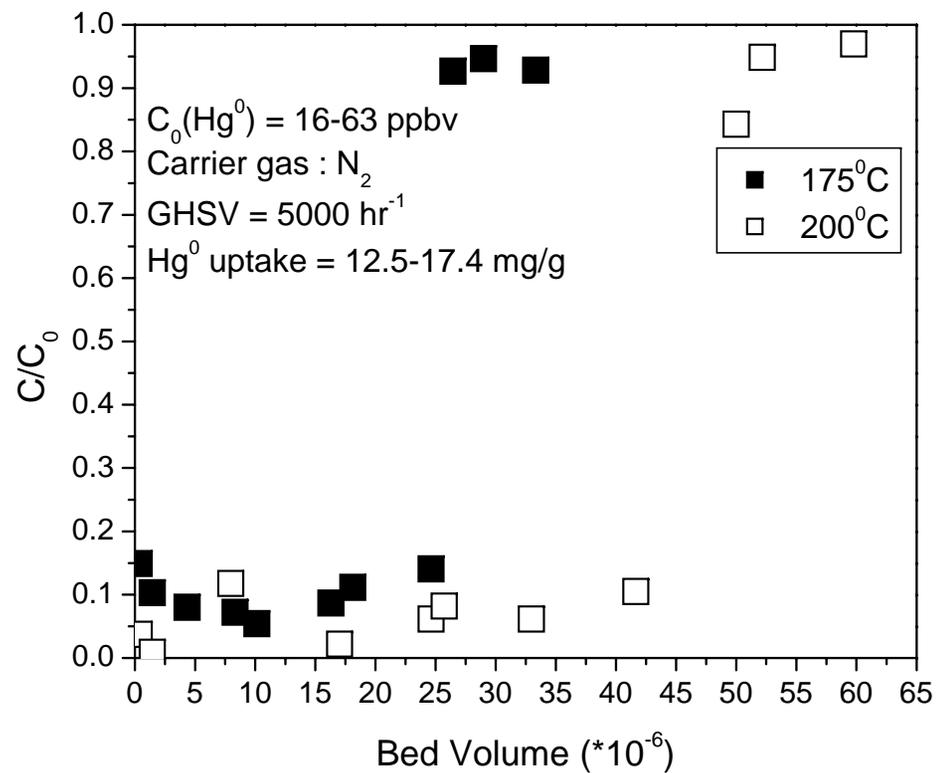


## XPS spectra of fresh and spent samples of 10 wt% MnO<sub>2</sub>/TiO<sub>2</sub> catalyst

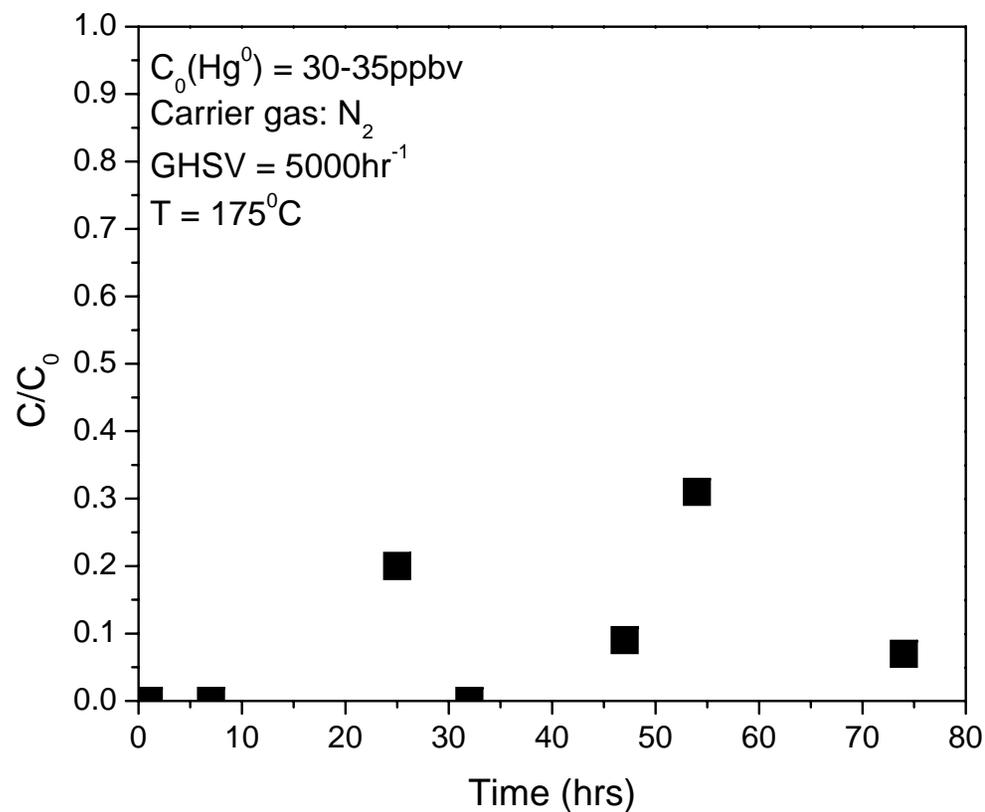


(A) Mn 2p XPS spectra for (a) fresh and (b) spent catalysts  
(B) Hg 4f XPS spectrum for spent catalyst

# Effect of Bed Temperature on Mercury Capture Behavior using 10wt% MnO<sub>2</sub> Catalyst



## Mercury Capture Behavior using 20wt% MnO<sub>2</sub> Catalyst after NO<sub>x</sub> Conversion



## Summary

- Remarkable mercury capacity was observed at 200 °C and inert atmosphere
- MnO<sub>2</sub>/TiO<sub>2</sub> catalysts are water tolerant. SO<sub>2</sub> has a negative effect on mercury capture
- Manganese loading and bed temperature were found to be important factor for mercury capture
- XPS results indicate that MnO<sub>2</sub>/TiO<sub>2</sub> are covered with mercury

## Acknowledgements

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- University of Cincinnati